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(a) Calculate the heat flux through the insulated sheet. Here, ΔT is the temperature difference, L is the length of the insulated sheet along the direction of heat flow, and k is the thermal conductivity. Substitute for, 0.02 m for L , and for k .

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This is consistent with the fact that the surface heat flux in the positive y -direction is given by the following equation: From the sketch, the temperature gradient is positive. Therefore, the heat flux is negative. The heat transfer is in the negative y -direction, the plate is being heated by the fluid.

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ASSUMPTIONS: (1) Steady-state conditions, (2) Negligible heat transfer from the wire by natural convection or radiation. ANALYSIS: If all of the electric energy is transferred by convection to the air, the following equality must be satisfied. $P_{elec} = hA(T_s - T_\infty)$ where $A = \pi DL$
($L = 0.0005\text{m}$, $D = 0.02\text{m}$, $h = 3.14 \times 10^4 \text{ W/m}^2\text{K}$, $T_s = 52 \text{ m}$). Hence, $h = \frac{P_{elec}}{\pi D L (T_s - T_\infty)}$

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FIND: (a) The heat flux through a 2 \square PROBLEM 1.1 KNOWN: Thermal conductivity, thickness and temperature difference across a sheet of rigid extruded insulation. Slideshare uses cookies to improve functionality and performance, and to provide you with relevant advertising.

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$dT/dx = -q/k$, is a constant, and hence the temperature distribution is linear. The heat flux must be constant under one-dimensional, steady-state conditions; and k is approximately constant if it depends only weakly on temperature. The heat flux and heat rate when the outside wall temperature is $T_2 = -15^\circ\text{C}$

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Assumptions 1 Steady operating conditions exist. 2 Convection heat transfer coefficient is uniform. 3 Heat transfer by radiation is negligible. 4 Heat losses from the boiler are negligible.

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